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**CLEAN COAL TECHNOLOGIES 2019**  
CONFERENCE 3-7 JUNE, HOUSTON

# Hg and SO<sub>2</sub> emission control potential of activated carbons based on brown coal and influence of material structure and composition

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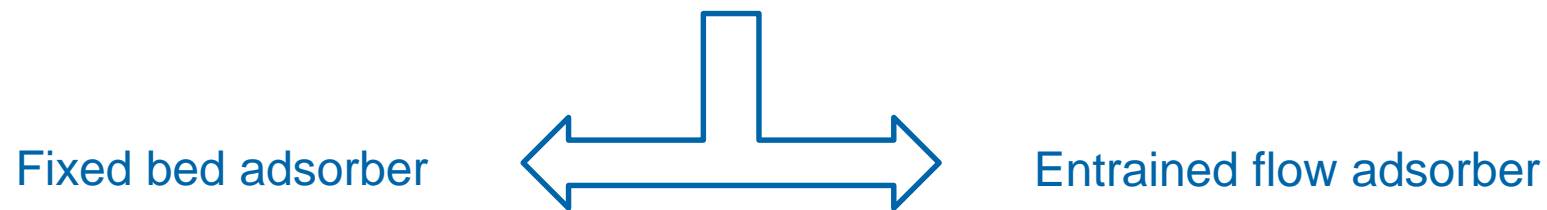
**03-07 June 2019**

# Outline

- 1 Motivation
- 2 Screening of feedstock
- 3 Optimization of carbon adsorbents production
- 4 Conclusion

## Increasing demands on activated carbons

- Power plant operators have to meet newly introduced emission limits in EU countries  
     e.g. mercury emissions from 2019: max.  $10 \mu\text{g}/\text{m}^3$
- Mercury emissions are mainly determined by used combustible material, influence of process parameters (lambda, boiler-temperature, etc.) is comparatively low
- Downstream applicable techniques have to be adopted



→ Different requirements towards properties of carbon adsorbents  
 e.g. grain size, impact resistance, ignition temperature, sorption rate,...

## Selection of feedstock

- Ideally, power plant companies can use their own coal as feedstock for carbon adsorbents
- Different coals from central german mining area were chosen
- Influence of grain size (fine and coarse) and mechanical pretreatment (granulation, pelletization) is determined
- Additionally, the influence of upstream material utilization on the product is evaluated, by sampling different stages of the wax extraction process from Romonta GmbH
- All in all 14 different feedstock products are investigated

2 dry coals (1 extracted), 2 raw coals,  
Pellets, electrostatic filter dust,  
5 fine granulates < 4 mm, 3 microgranulates < 1 mm (1 extracted)

# Determination of suitability for production of carbon adsorbents

## Feedstock characterization + thermochemical behaviour

- Proximate + ultimate analysis
- LHV + HHV
- XRF
- Hg-porosimetry + He-pyknometrie (apparent and skeletal density, pore size distribution)
- Mass loss curves via TG-DSC
- Fixed bed pyrolysis (mass balance and product yields)

## Production of carbon adsorbents using constant process conditions

- Retorte furnace
- Process conditions in analogy to HOK®
  - High heating rate (app. 40 K/min)
  - Bed temperature ~ 950 °C
  - Dwell time 60 min
  - Fast cooling under water vapor
  - Injection of air below 120 °C

→ low activation rate and oxidation

## Characterization of adsorption relevant properties + Benchmark

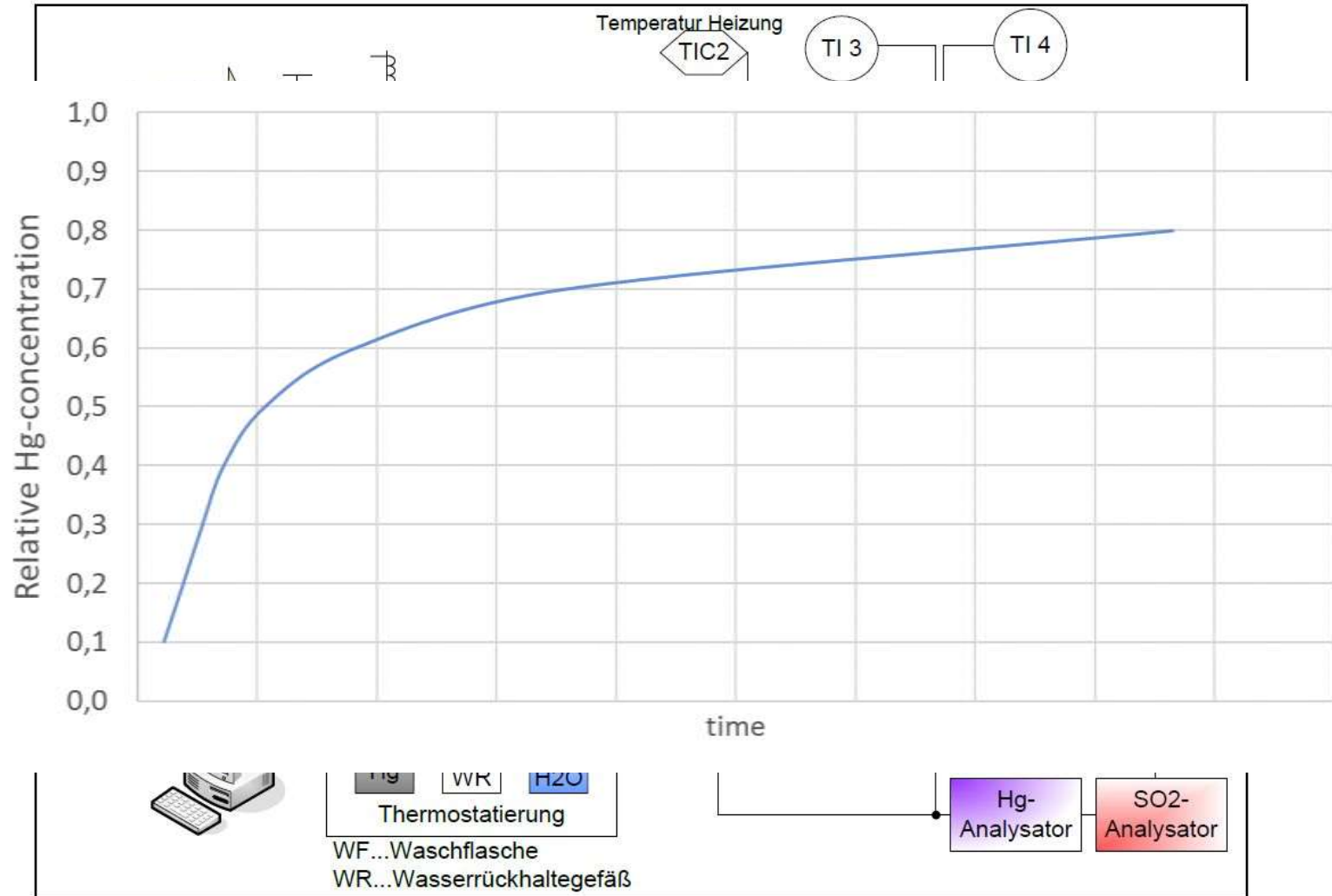
- Proximate + ultimate analysis
- Hg-porosimetry + He-pyknometrie
- Reactivity towards CO<sub>2</sub>
- Impact resistance
- Ignition temperature
- Burning number
- Inner specific surface area (BET)
- Iodine number
- Methylene-blue number
- Adsorption characteristics (Hg/SO<sub>2</sub>)

→ Benchmark: HOK® products from RWE  
granulate, medium, dust and super

## Determination of adsorption performance

- Heated fixed bed reactor
- Appr. 10 g sample mass
- T ~ 140 - 160 °C
- Simulated flue gas
- 600 µg/m<sup>3</sup> Hg / 400 ppm SO<sub>2</sub>
- Constant measuring of Hg/SO<sub>2</sub>-concentration

→ Results: dynamic adsorption capacity, breakthrough time, inhibitive influences of flue gas



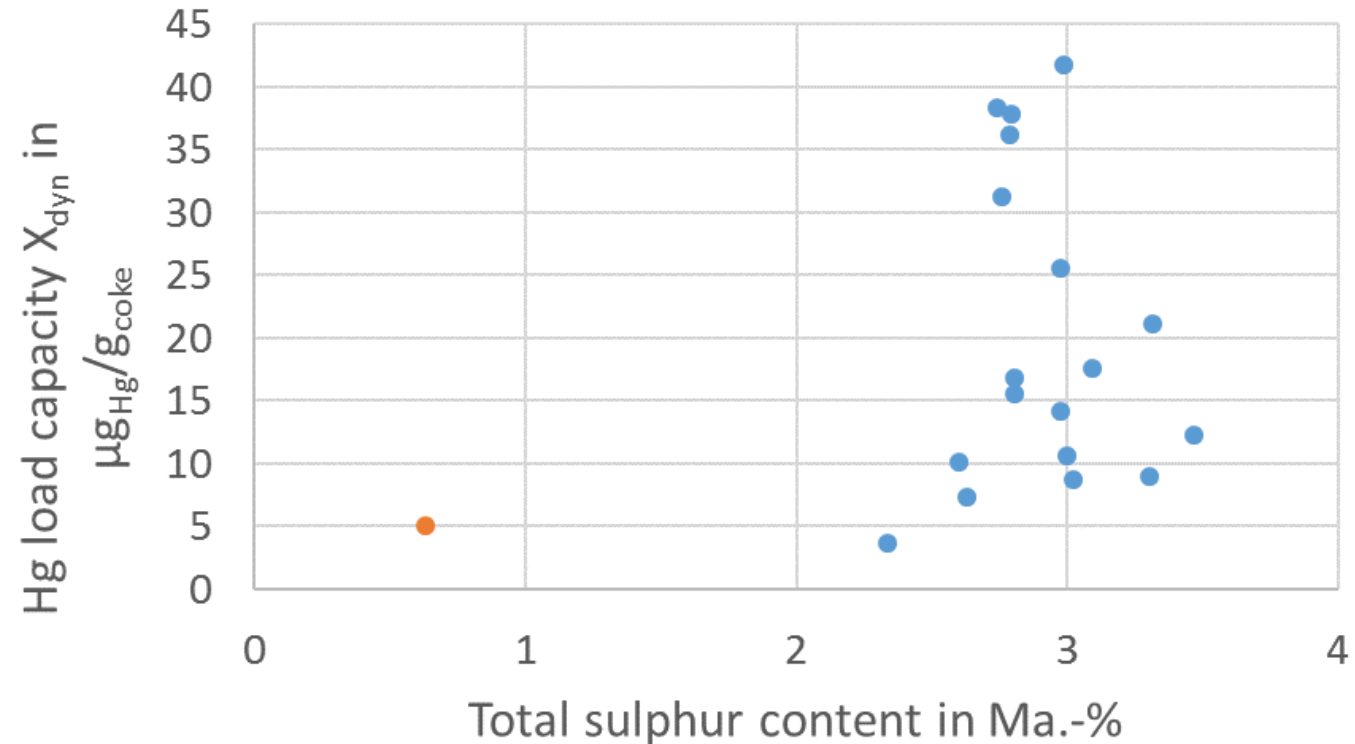
## Results

- Retorte furnace adsorbents show superior adsorption behaviour compared to ● HOK®
- Similar burning behaviour
- Lower values for ignition point, impact resistance and reactivity
- Increased adsorption behaviour is observed
- Lower inner specific areas are created

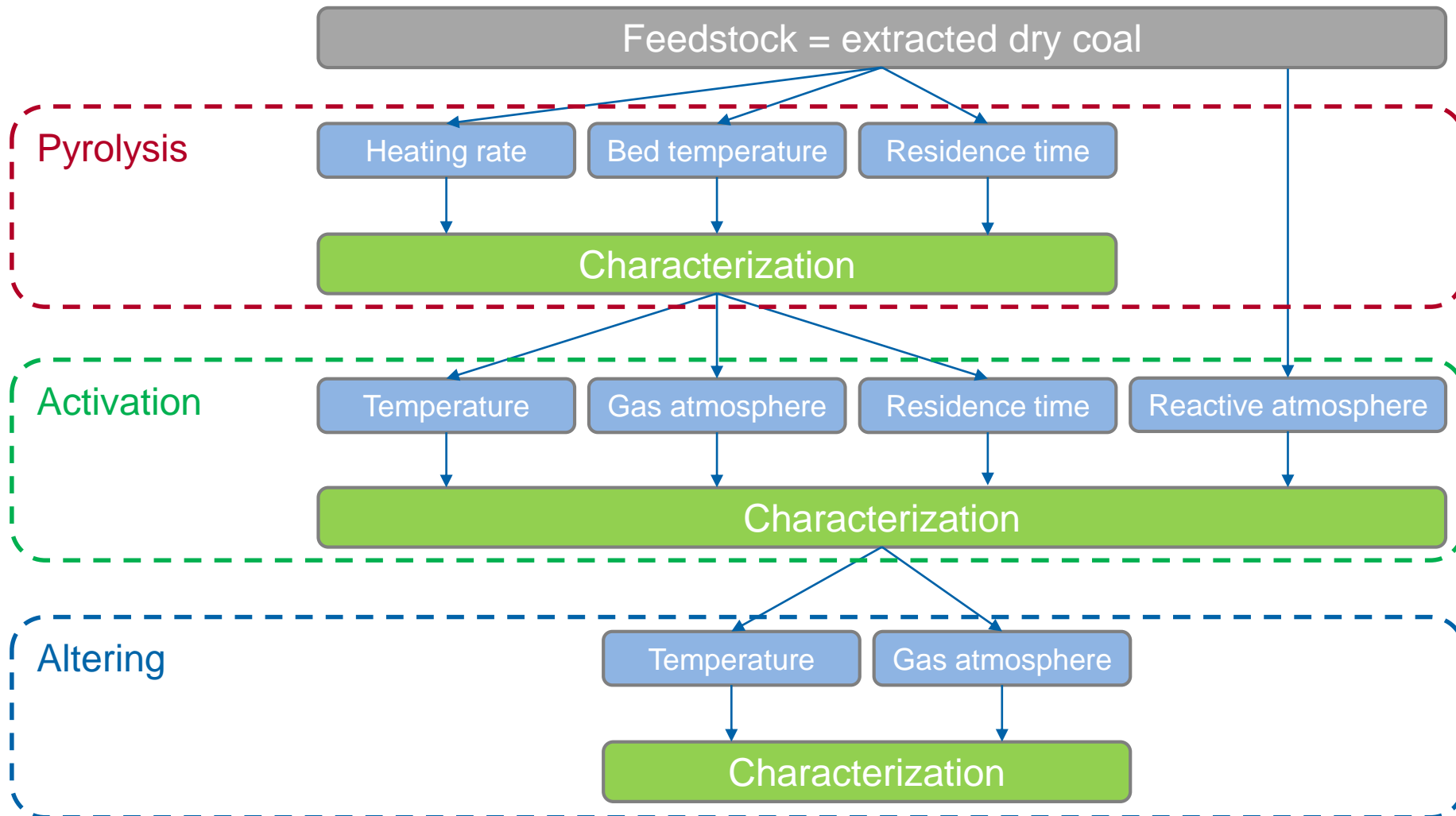
→ Sulphur content of coke is essential for mercury adsorption

→ gas activation is indicated for higher porosity and inner specific surface area

Hg adsorption capacity vs. total sulphur content



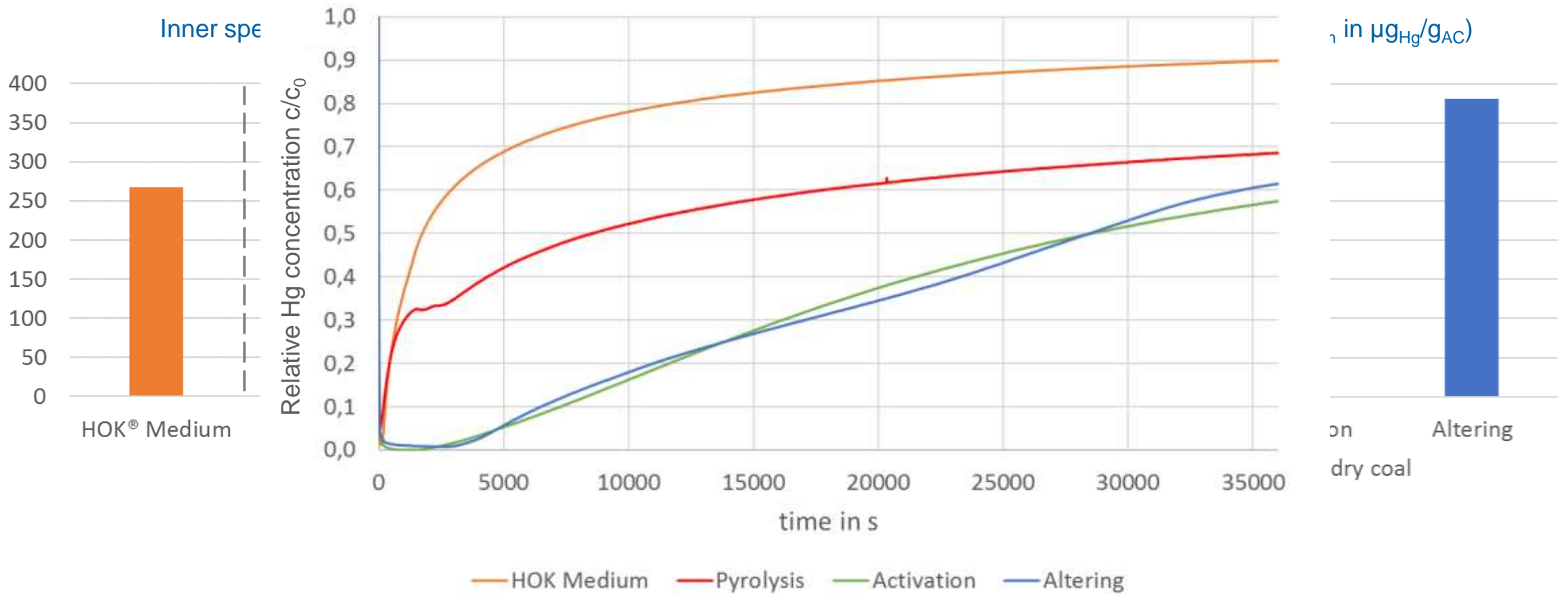
# Variation of process parameters - pyrolysis, activation and altering



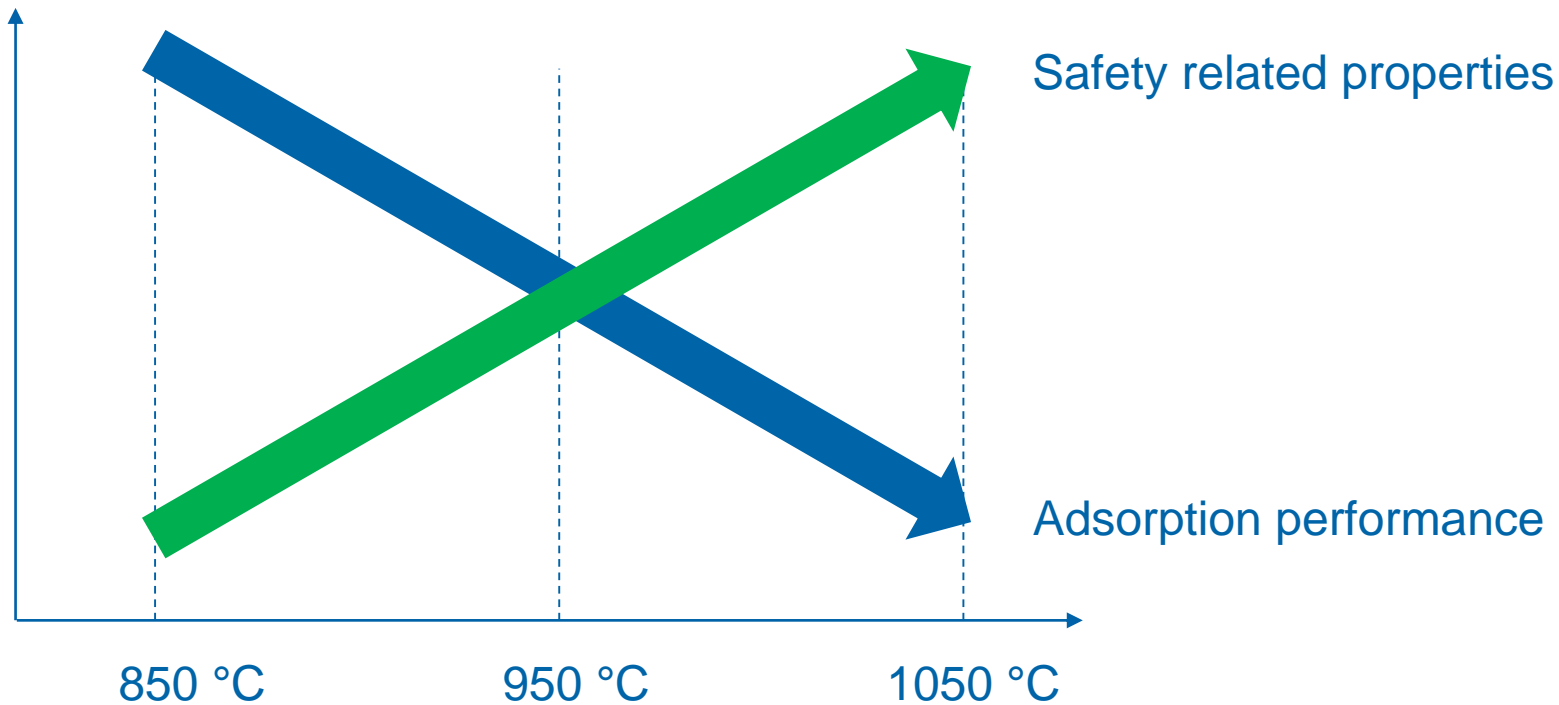


# Results of parameter variation

Relative Hg concentration over time



## Results of parameter variation



→ optimal parameters for carbon adsorbents production assessable

## Conclusion

# Properties of possible products

- High-quality and competitive carbon adsorbents from Romonta feedstock materials are fabricable
- Relevant properties regarding adsorption performance and safety-related characteristics exceed the values of HOK®
- Upstream granulation process is essential for impact resistance, a former extraction process is non-constraining applicable

| Parameter                             | AC from extracted dry coal | HOK® Medium                | AC from fine granulate     |
|---------------------------------------|----------------------------|----------------------------|----------------------------|
| Porosity                              | 52 %                       | 55 %                       | 46 %                       |
| Inner specific surface area (BET)     | 351 m <sup>2</sup> /g      | 267 m <sup>2</sup> /g      | 395 m <sup>2</sup> /g      |
| Iodine number                         | 285 mg I <sub>2</sub> /g   | 325 mg I <sub>2</sub> /g   | 310 mg I <sub>2</sub> /g   |
| Impact resistance                     | 46 %                       | 52 %                       | 65 %                       |
| Ignition temperature                  | 325 °C                     | 345 °C                     | 310 °C                     |
| Burning number                        | 4                          | 3                          | 4                          |
| Reactivity                            | 1 cm <sup>3</sup> /(g s)   | 1,8 cm <sup>3</sup> /(g s) | 1,3 cm <sup>3</sup> /(g s) |
| Methylene-blue number                 | 2,5 ml                     | 3 ml                       | 2 ml                       |
| Hg-adsorption capacity*               | 38,4 µg/g                  | 5,1 µg/g                   | 36 µg/g                    |
| SO <sub>2</sub> -adsorption capacity* | 33,5 mg/g                  | 3,5 mg/g                   | 36,1 mg/g                  |

→ single-use carbon adsorbents for gas treatment in granulated and powdered form are feasible

## Acknowledgement

The results of this presentation were gathered from the AiF (The German Federation of Industrial Research Associations) funded project „Production of high quality carbon products based on extracted coals“ within the scope of ZIM funding programm (central innovation program for medium-sized businesses).



# ROMONTA

